



# Fluxus Natural Gas Engine

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# Content

Introduction

Natural Gas Engine Capabilities

Conclusions

References

# Flexim Company History

## Headquarter in Berlin

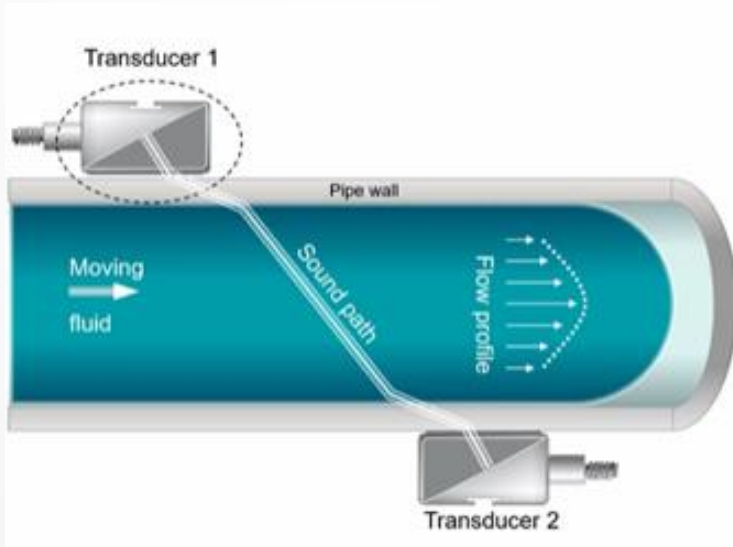
- 270 employees
- Manufacturing, calibration, research & development
- All shareholders are company founders
- Technology driven development



## Global Company

- Branches worldwide
- Final production, service support points and calibration facilities in target markets
- Approximately 500 direct FLEXIM employees worldwide
- Extensive Representative and Distributor Network

# Ultrasonic Meters Sound Speed Principle



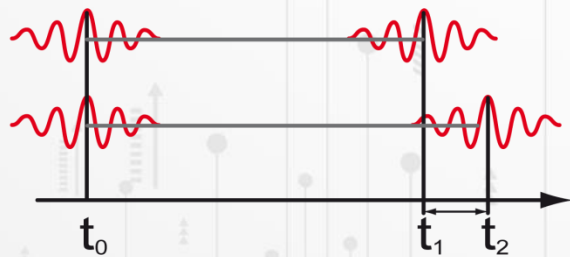
**Ultrasonic flow meters can measure sound speed and flow simultaneously:**

**Sonic velocity:**

$$c_{Fluid} = \frac{l_{Fluid}}{\frac{t_{down} + t_{up}}{2} - t_0}$$

**Volume flow:**

$$Q = K_{Re} \cdot A \cdot K_{\alpha} \frac{\Delta t}{2t_{fl}}$$



# Introduction to Fluxus Natural Gas Engine

- USM Gas Measurement is widely accepted in the Oil & Gas Industry, however, changes in gas composition can have an effect in meter accuracy and require additional field instrumentation to convert meter output from actual to standard conditions.
- Since natural gas is a multicomponent, not ideal gas, compressibility factor calculations are challenging and require knowledge of gas composition.
- Traditionally, the process of estimating the Z-factor involved empirical correlations, which often yielded weak results either due to their limited accuracy or due to calculation difficulties, therefore;

**Gas Chromatographer and a Flow Computers are used for:**

1. **Unit conversion from actual to standard conditions**
2. **Calculate gas compressibility factor Z**
3. **Molecular weight**
4. **Density & Calorific Values**

$$Z = \frac{PV}{nRT}$$

*Not Applicable*

# Actual to Standard Conversion for Gases

- AGA-9 is the standard for ultrasonic gas flow measurement
- AGA-9 formula for Standard Volume:
- STD volume is compensated for pressure – temp - compressibility

$$Q_b = \underline{Q_f} (P_f/P_b) (T_b/T_f) (Z_b/Z_f)$$

Where:

$Q_b$	=	Flow rate at base conditions
$Q_f$	=	Flow rate at flowing conditions
$P_b$	=	Base pressure, typically 14.73 psia (101.325 kPa)
$P_f$	=	Absolute static pressure of gas at flowing conditions from meter tap
$T_b$	=	Base temperature, typically 519.67 °R (288.15 °K)
$T_f$	=	Absolute temperature of gas at flowing conditions
$Z_b$	=	Compressibility factor of gas at base conditions, per A.G.A. Report No. 8
$Z_f$	=	Compressibility factor of gas at flowing conditions, per A.G.A. Report No. 8



# Software – Calculates Z (compressibility)

## Standard Natural Gas Example

AGA 10 Example Program

File Help

Composition (Mole Percent)

Helium	0.	Propane	0.2002002	n-Octane	0.
Hydrogen	0.	i-Butane	0.	n-Nonane	0.
Nitrogen	1.3013013	n-Butane	0.	n-Decane	0.
CO2	0.	i-Pentane	0.	Argon	0.
H2S	0.	n-Pentane	0.	Water	0.
Methane	95.2952953	n-Hexane	0.	CO	0.700700701
Ethane	2.5025025	n-Heptane	0.	O2	0.

Clear Mixture Normalize TOTAL 100.000000

Gas Temperature and Absolute Pressure

Pb 14. PSI Pf 800. PSI

Tb 60. Fahrenheit Tf 70. Fahrenheit

Current Status

Calculation Completed

Initialize Calculate Quit

Calculation Results

Speed of Sound	423.149582	metres per second
C*	0.710929278	
Isentropic Exponent	1.35669684	
Specific Enthalpy	536.437251	kJ per kg
Specific Entropy	9.20143751	kJ per kg-K
Molar Density	2.50410433	moles/dm3
Mass Density	41.7930388	kg per cubic metre
RD (ideal gas)	0.576254838	
RD (real gas)	0.577152314	
Zb	0.998050593	
Zf	0.900299523	
Fpv	1.05288944	
Molar Mass	16.6898153	
Cp (ideal gas)	2.15234239	kJ/kg-K
Cp (real gas)	2.56831374	kJ/kg-K
Cv (real gas)	1.71724329	kJ/kg-K
Cp/Cv	1.49560272	
Enthalpy (ideal gas)	593.605441	kJ/kg

## Low Methane Content Example

AGA 10 Example Program

File Help

Composition (Mole Percent)

Helium	0.	Propane	2.3015	n-Octane	0.
Hydrogen	0.	i-Butane	0.3486	n-Nonane	0.
Nitrogen	1.0068	n-Butane	0.3506	n-Decane	0.
CO2	1.4954	i-Pentane	5.09e-002	Argon	0.
H2S	0.	n-Pentane	4.8e-002	Water	0.
Methane	85.9063	n-Hexane	0.	CO	0.
Ethane	8.4919	n-Heptane	0.	O2	0.

Clear Mixture Normalize TOTAL 100.000000

Gas Temperature and Absolute Pressure

Pb 14.7 PSI Pf 800. PSI

Tb 60. Fahrenheit Tf 70. Fahrenheit

Current Status

Press Calculate

Initialize Calculate Quit

Calculation Results

Speed of Sound	386.255707	metres per second
C*	0.718718989	
Isentropic Exponent	1.32237785	
Specific Enthalpy	477.115509	kJ per kg
Specific Entropy	8.59607446	kJ per kg-K
Molar Density	2.6048962	moles/dm3
Mass Density	48.8894012	kg per cubic metre
RD (ideal gas)	0.648018418	
RD (real gas)	0.649489417	
Zb	0.997315735	
Zf	0.86546402	
Fpv	1.07347473	
Molar Mass	18.7682723	
Cp (ideal gas)	2.03978969	kJ/kg-K
Cp (real gas)	2.55315087	kJ/kg-K
Cv (real gas)	1.68099457	kJ/kg-K
Cp/Cv	1.51883351	
Enthalpy (ideal gas)	542.634107	kJ/kg

# Speed of Sound Changes Based On Gas Composition

- The speed of sound in natural gas is the velocity a sound wave travels in the gas.
- Properties of different gases such as composition, P&T affect the speed of sound
- Uncertainty in Compressibility factor = decreased accuracy

**AGA 10 States:**  
**“One of the USM meter diagnostics is comparing the speed of sound determined by the meter to the theoretical speed of sound in the gas as calculated by AGA Report No. 10.”**

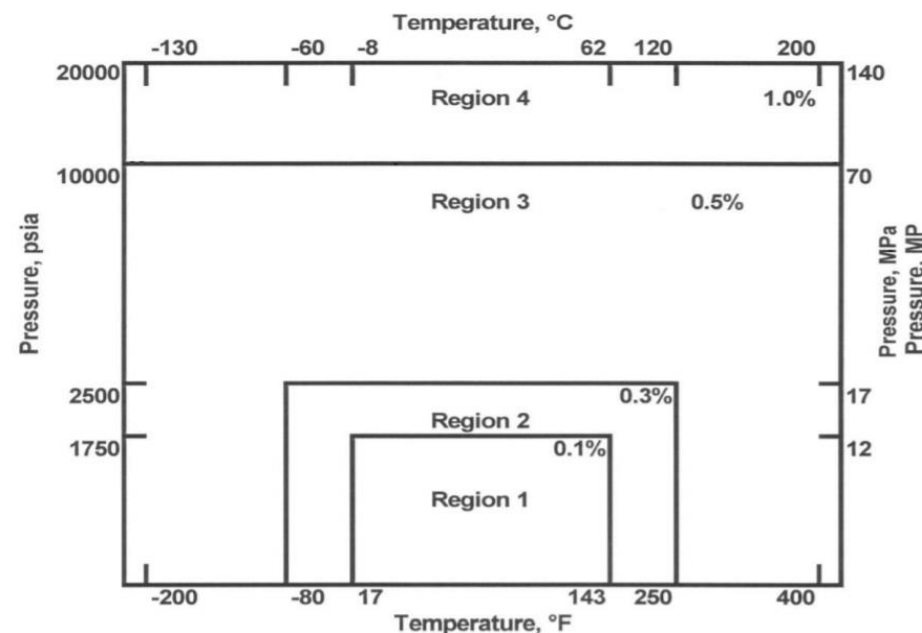


Figure 1: Targeted Uncertainty for Natural Gas Speed of Sound Using the AGA Report No. 10 Method



# Typical Effect on SoS of P&T changes VS Composition Changes

TEMP → PRESS ↓	30°F	31°F	35°F	40°F	60°F	70°F	90°F	100°F	120°F
200 PSIG	1351.1	1352.6	1358.5	1365.9	1394.4	1408.3	1435.1	1448.1	1473.4
201 PSIG	1351.0	1352.5	1358.4	1365.8	1394.3	1408.2	1435.0	1448.0	1473.4
202 PSIG	1350.9	1352.4	1358.3	1365.7	1394.3	1408.1	1434.9	1448.0	1473.3
205 PSIG	1350.5	1352.0	1358.0	1365.4	1394.0	1407.9	1434.8	1447.8	1473.2
210 PSIG	1350.0	1351.5	1357.5	1364.9	1393.6	1407.5	1434.4	1447.5	1472.9
500 PSIG	1321.6	1323.4	1330.4	1339.1	1372.4	1388.4	1418.9	1433.6	1461.9
501 PSIG	1321.5	1323.3	1330.3	1339.0	1372.4	1388.3	1418.9	1433.6	1461.9
502 PSIG	1321.4	1323.2	1330.3	1338.9	1372.3	1388.3	1418.8	1433.5	1461.9
505 PSIG	1320.7	1323.0	1330.0	1338.7	1372.1	1388.1	1418.7	1433.4	1461.8
510 PSIG	1320.7	1322.5	1329.6	1338.3	1371.8	1387.8	1418.5	1433.3	1461.7
1000 PSIG	1296.3	1298.4	1306.8	1317.1	1356.2	1374.6	1409.7	1426.4	1458.3
1001 PSIG	1296.3	1298.4	1306.8	1317.0	1356.2	1374.6	1409.7	1426.4	1458.3
1005 PSIG	1296.2	1298.4	1306.7	1317.0	1356.2	1374.7	1409.7	1426.4	1458.4
1010 PSIG	1296.2	1298.3	1306.7	1317.0	1356.2	1374.7	1409.7	1426.5	1458.5

Table 2 Speed of Sound in Ft/Sec

Components in Mole Percent	Gulf Coast Gas	Ekofisk Gas	Amarillo Gas	Air
Speed of Sound @14.73 & 60°F	1412.4	1365.6	1377.8	1118.05
G <sub>r</sub>	0.581078	0.649521	0.608657	1.00
Heating Value	1036.05	1108.11	1034.85	
Methane	96.5222	85.9063	90.6724	
Nitrogen	0.2595	1.0068	3.1284	78.03
Carbon Dioxide	0.5956	1.4954	0.4676	0.03
Ethane	1.8186	8.4919	4.5279	
Propane	0.4596	2.3015	0.8280	
i-Butane	0.0977	0.3486	0.1037	
n-Butane	0.1007	0.3506	0.1563	
i-Pentane	0.0473	0.0509	0.0321	
n-Pentane	0.0324	0.0480	0.0443	
n- Hexane	0.0664	0.0000	0.0393	

Table 3 Reference Gas Compositions

# Content

Introduction

Natural Gas Engine Capabilities

Conclusions

References

# Fluxus - Natural Gas Engine Principle

- SoS and Thermodynamic variables applied to calculate Z, MW and HHV derived from pressure and temperature inputs under operating conditions.
- Standard unit conversion calculated dynamically withing the Fluxus meter
- Natural gases are divided into classes based on their HHV in MJ/Kg
- No need to know exact gas composition
- HHV calculation requires known % of N<sub>2</sub> & CO<sub>2</sub>

## Class 2. High HHV – NGE - H

name	min	mean	max
temperature [°C]	-1	30	81
pressure [bar]	0.4	63	98
HHV [MJ/kg]	43	51.9	54.7
mol. weight [g/mol]	16.7	18.9	30.8
methane [mol%]	42	87.1	97.1
ethane [mol%]	0.3	7.0	23.7
propane [mol%]	0.01	2.1	15.5
i-butane [mol%]	0	0.47	3.9
n-butane [mol%]	0	0.47	5.3
i-pentane [mol%]	0	0.16	1.44
n-pentane [mol%]	0	0.1	1.3
n-hexane [mol%]	0	0.13	1.02
n-heptane [mol%]	0	0.07	0.37
C8 & more [mol%]	0	0.02	0.21
O <sub>2</sub> [mol%]	0	0	0.22
N <sub>2</sub> [mol%]	0.08	0.44	6.97
CO <sub>2</sub> [mol%]	0	1.99	10.3

## Class 3. High HHV – NGE - L

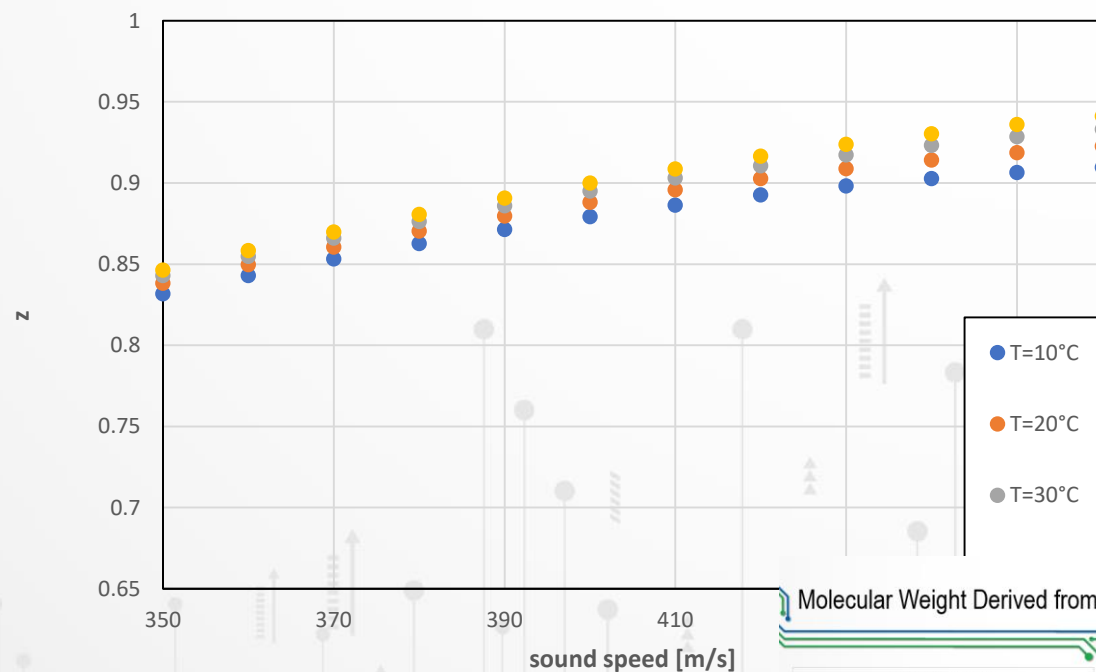
Name	min	mean	max
temperature [°C]	3	26	85
pressure [bar]	5	42	95
HHV [MJ/kg]	25	35.3	43.4
mol. weight [g/mol]	20.7	23.3	26.8
methane [mol%]	60.1	72.3	91.9
ethane [mol%]	2.34	5.02	9.74
propane [mol%]	0.69	1.87	3.81
i-butane [mol%]	0.15	0.42	0.93
n-butane [mol%]	0.14	0.51	1.09
i-pentane [mol%]	0.05	0.18	0.44
n-pentane [mol%]	0.03	0.14	0.32
n-hexane [mol%]	0.02	0.17	0.46
n-heptane [mol%]	0.01	0.09	0.22
C8 & more [mol%]	0	0.02	0.07
O <sub>2</sub> [mol%]	0	0	0.03
N <sub>2</sub> [mol%]	0.33	0.84	1.67
CO <sub>2</sub> [mol%]	10.3	18.4	32.8

## Class 4. High HHV – NGE - F

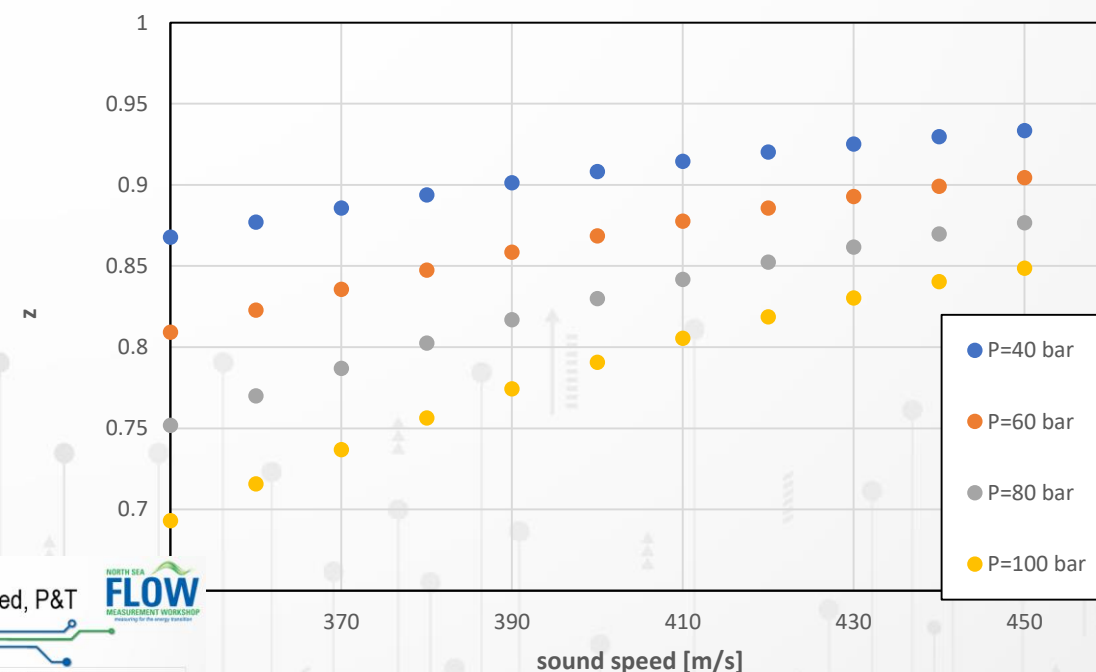
Name	min	mean	Max
temperature [°C]	10	28	52
pressure [bar]	0.05	6.3	53
HHV [MJ/kg]	1.9	16.2	53.2
mol. weight [g/mol]	17.3	31.8	41.6
methane [mol%]	8.1	42.9	95.0
ethane [mol%]	0.15	1.48	8.32
propane [mol%]	0.02	0.29	2.91
i-butane [mol%]	0	0.07	0.76
n-butane [mol%]	0	0.09	0.70
i-pentane [mol%]	0	0.03	0.39
n-pentane [mol%]	0	0.03	0.72
n-hexane [mol%]	0	0.06	3.05
n-heptane [mol%]	0	0.06	1.92
C8 & more [mol%]	0	0.02	0.32
O <sub>2</sub> [mol%]	0	0.01	0.64
N <sub>2</sub> [mol%]	0.18	0.75	3.29
CO <sub>2</sub> [mol%]	0	54.3	90.6

# Compressibility (**Z Factor**) Derived from Sound Speed, P&T

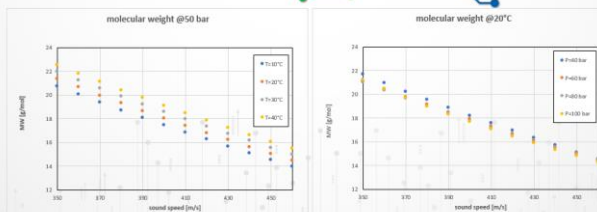
compressibility @50 bar



compressibility @20°C

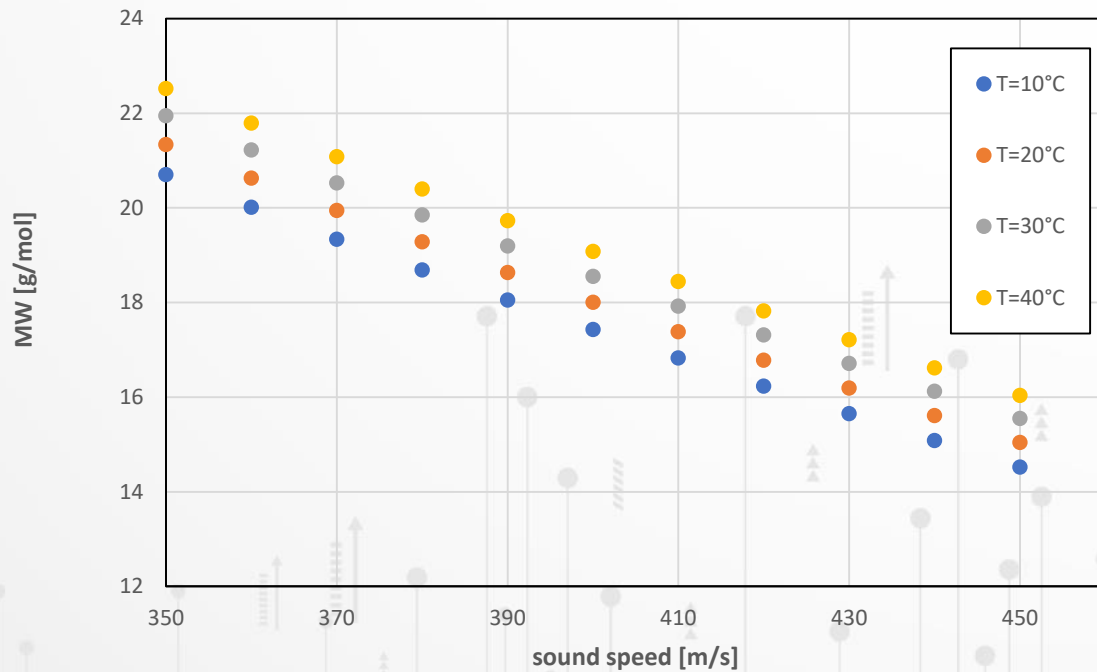


Molecular Weight Derived from Sound Speed, P&T

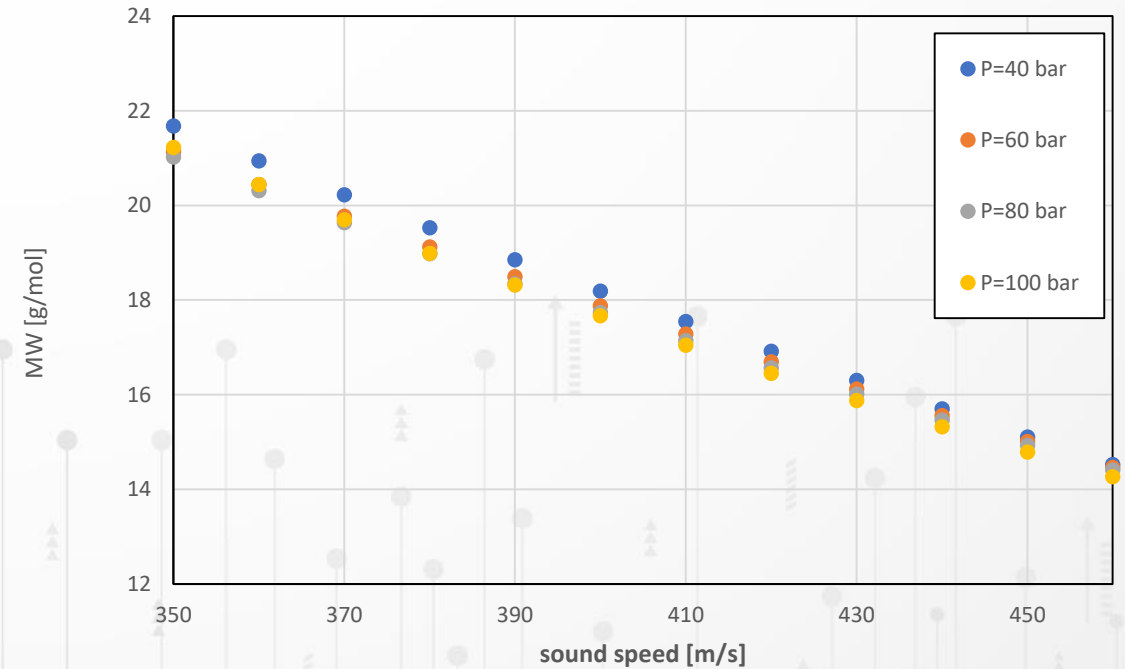


# Molecular Weight Derived from Sound Speed, P&T

molecular weight @50 bar



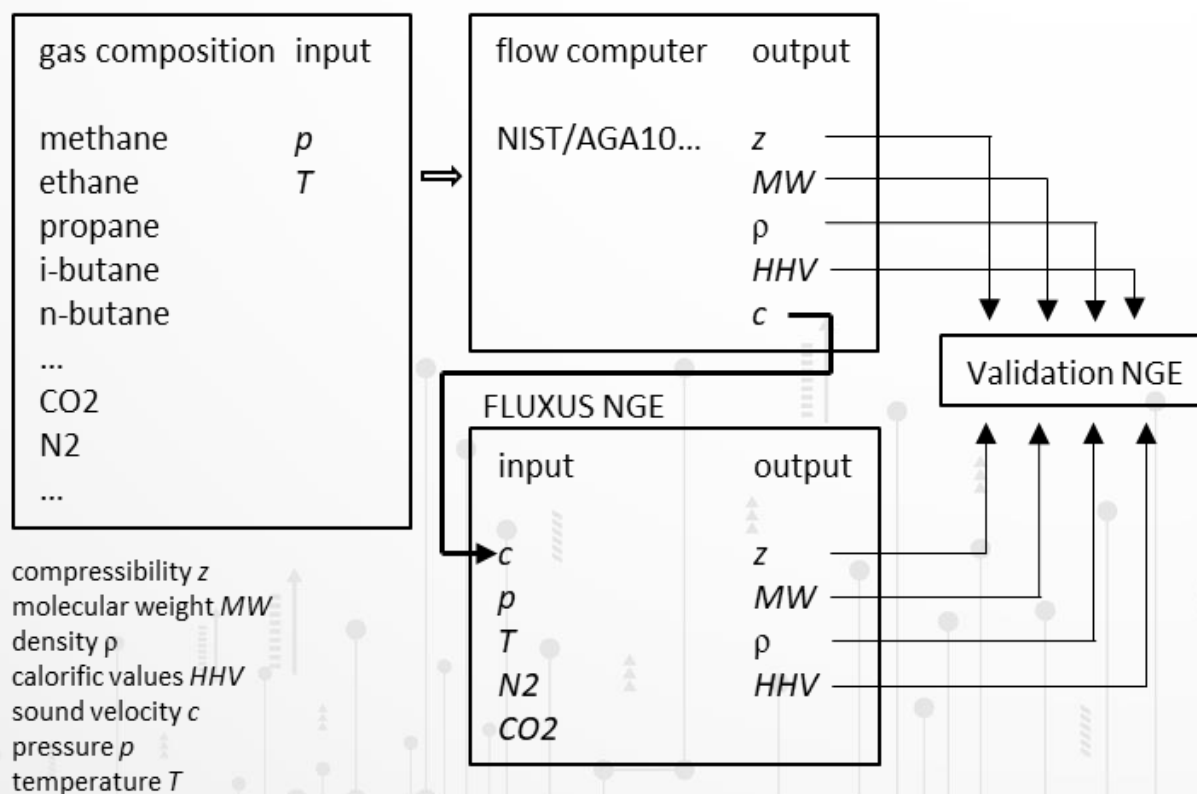
molecular weight @20°C



# Fluxus - Natural Gas Engine Principle

## Industry-standard method vs. NGE

gas chromatograph + flow computer



## Internal Calculations derived from SoS

- $z_{NGE} = z(c, T, p)$
- $MW_{NGE} = MW(c, T, p)$
- $HHV_{NGE} = HHV(c, MW, N_2, CO_2)$

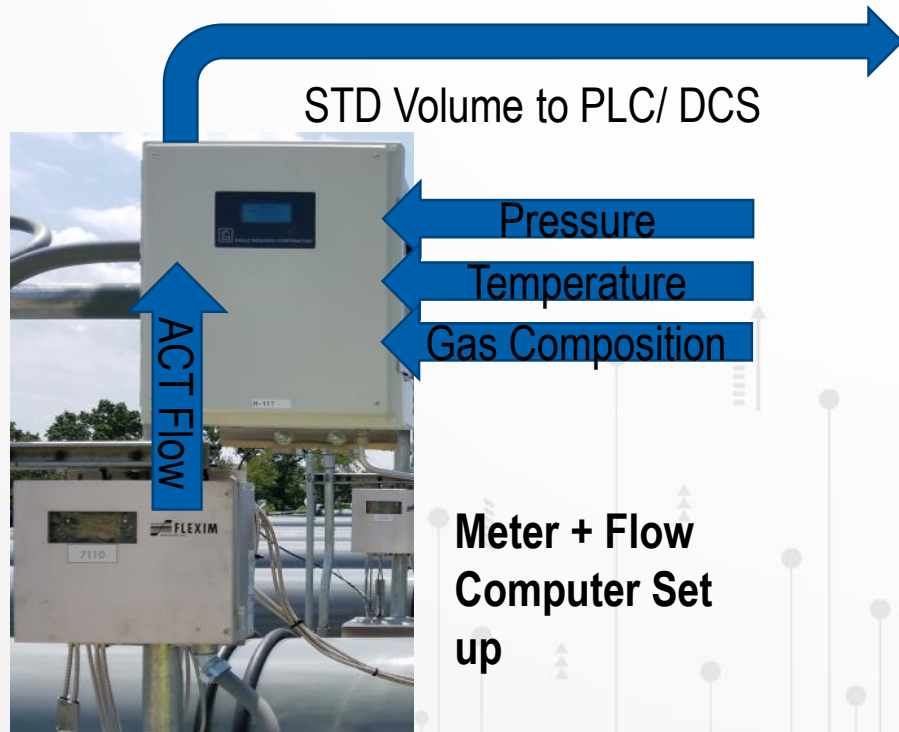
## Measurement uncertainties

- Technical specs of P&T Sensors
- Sound velocity uncertainty of Fluxus Clamp on meter
- Meter installation & Sensitivity coefficients

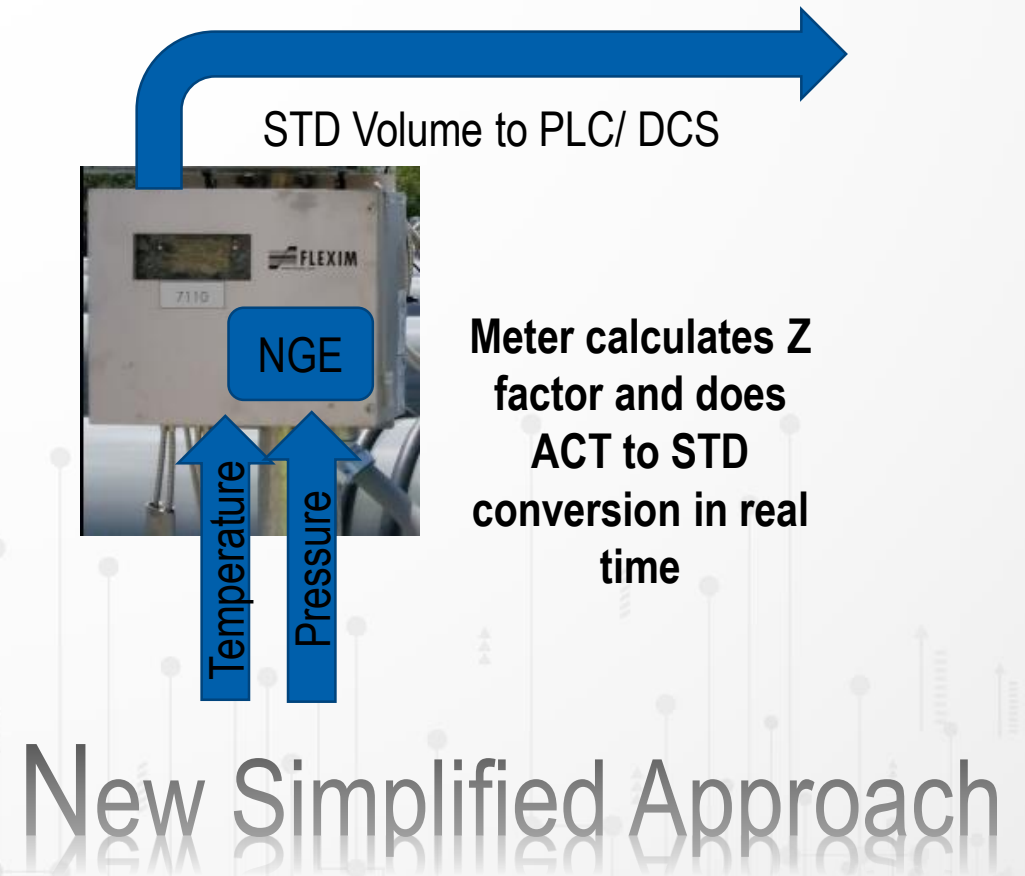


# Natural Gas Engine Replaces Flow Computer

## Standard methodology



VS



# NGE Accuracy Results Comparison Vs Flow Comp.

Compressibility  $z$  and MW for NGE vs. flow computer

	class 2	class 3	class 4
sample std. dev. $z_{\text{NGE}}$	0.7%	0.9%	0.4%
data points within 1%	84.3%	80.3%	96.2%
data points within 2%	97.6%	91.0%	99.5%
data points >3% off	0.1%	0.7%	0%
sample std. dev. $MW_{\text{NGE}}$	1.1%	1.3%	1.1%
data points within 1%	59.0%	65.3%	85.8%
data points within 2%	90.4%	85.3%	92.9%
data points >3% off	3.5%	4.7%	4.4%

HHV for NGE vs. flow computer

	class 2	class 3	class 4
sample std. dev. HHV in MJ/kg	0.7%	1.2%	3.4%
data points within 1%	85.1%	52.3%	19.7%
data points within 2%	98.8%	85.7%	29.0%
data points >3% off	0.0%	1.7%	19.1%
sample std. dev. HHV in MJ/m <sup>3</sup>	1.4%	2.3%	4.6%
data points within 1%	59.1%	33.3%	20.8%
data points within 2%	88.2%	61.7%	31.2%
data points >3% off	5.0%	26.7%	19.1%

Over 2000 measuring points were evaluated and compared to Flow Computer outputs to determine deviation.

# How Does Class Selection Affect NGE Calculations?

P [bar]	60
T [°C]	20

		nitrogen	CO2	methane	ethane	propane	isobutane	butane	isopentane	pentane	hexane	heptane	octane
Ref. Gas H	Nordsee H	0.009	0.019	0.863	0.086	0.019	0.000	0.000	0.000	0.000	0.000	0.000	0.000
Ref. Gas L	Ingreso a Planta ADLA	1.287	18.537	74.442	3.303	1.209	0.251	0.400	0.158	0.131	0.167	0.095	0.021

## Z & MW Results

FLUXUS measure	NIST		NGE correct gas class		NGE wrong gas class	
c	Z	MW	Z	MW	Z	MW
[m/s]		[g/mol]		[g/mol]		[g/mol]
390.78	0.860	18.43	0.860	18.64	0.890	18.70
346.90	0.842	22.84	0.840	22.48	0.805	22.01

NGE vs NIST Z Factor calculation with +/- 0.6% deviation

## HHV Results

NIST	NGE correct gas class	NGE wrong gas class
HHV	HHV	HHV
[MJ/kg]	[MJ/kg]	[MJ/kg]
51.56	51.6	54
34.30	34.2	32.1

NGE vs NIST HHV Factor calculation with +/- 0.3% deviation

# Content

Introduction

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Conclusions

References

# Conclusion

1. Fluxus NGE embedded feature in Clamp On Ultrasonic Meter
2. Enables real time dynamic gas compressibility calculation without a known composition input
3. Performs actual to standard conversion without flow computer.
4. Live line pressure and temperature inputs required
5. 3 main gas classes for end user to select based on HHV
6. MW and HHV calculations possible with known N2 and CO2 content

# Content

Introduction

Natural Gas Engine Capabilities

Conclusions

References



# References

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