

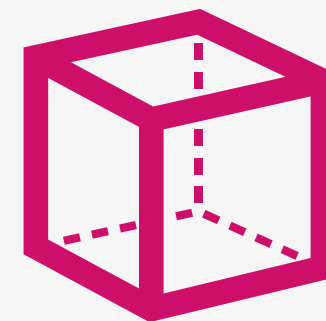
Small details, big impact

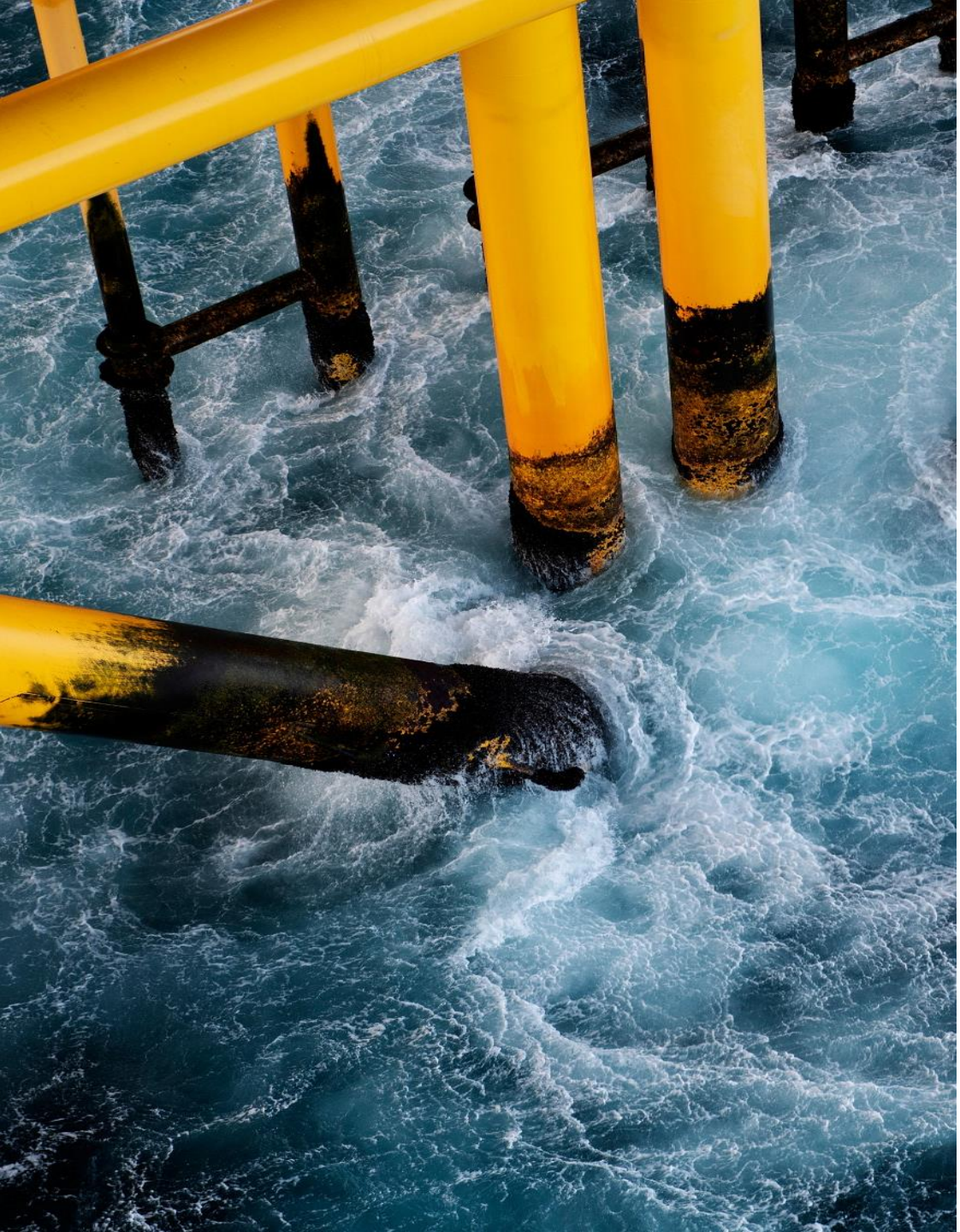
Practical examples of commercial and technical drivers in allocation

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To barrel or not to barrel...

- BOE
- OE
- Which unit did you express the tariff basis in in your last agreement?
 - $1 \text{ Sm}^3 \text{ water [BOE]} = 0 \text{ MJ}$
 - $1 \text{ Sm}^3 \text{ water [OE]} = 1 \text{ Sm}^3$
 - $1 \text{ Sm}^3 \text{ water [OE in barrels]} = 6.29 \text{ bbl}$
- ...or did you *forget* water in your tariff agreement?





Who will pay the water bill?

- Tariff per redelivered oil and gas volumes, not throughput
- Water production can vary gravely across fields
- WLR of a stream becomes considerable with field's age
- Processing of produced water is resource-demanding
 - One of the highest specific heat capacity of any liquid on Earth
 - Temperature of well streams from same reservoir can span over 80°C
 - Major driver of electrical power consumption: heating and injection
- Example:

	Sm ³	OE	OE in bbl	Water Liquid Ratio
Oil export	150 000	150 000	943 500	65%
Gas export	35 000 000	35 000	220 150	
Prod. water	280 000	280 000	1 761 200	

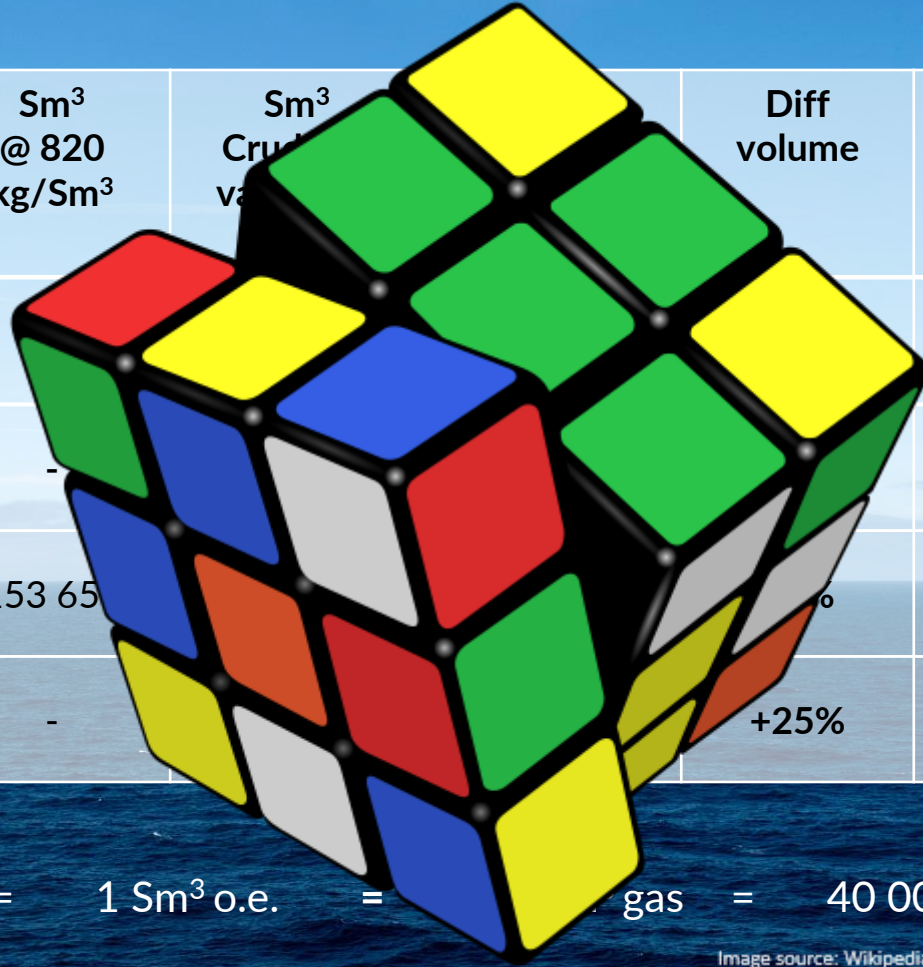
To muddy the waters...

	Sm³	OE in bbl	Tariff 1	Invoice 1	BOE	Tariff 2	Invoice 2
Oil export	150 000	943 500	15 NOK/bbl	14 152 500	943 500	15 NOK/BOE	14 152 500
Gas export	35 000 000	220 150		3 302 250	277 713		4 165 695
Prod. water	280 000	1 761 200		26 418 000	0		0
SUM [NOK]				43 872 750			18 668 040

A cube is not just a cube...

Allocated values
 Gas: 35 000 000 Sm³
 Oil: 150 000 Sm³

	Sm ³ normalized to 40 GCV	Sm ³ enriched with NGL to 55 GCV	Sm ³ @ 820 kg/Sm ³	Sm ³ Crude value	Diff volume	BOE	Diff value
Gas	42 475 213	-	-	-	-	277 713	0%
Gas	-	34 190 711	-	-	-	307 377	+11%
Oil	-	-	153 65	-	-	966 512	+2%
Oil	-	-	-	-	+25%	1 179 375	+25%



1 Sm³ oil = 35 500 MJ = 1 Sm³ o.e. = gas = 40 000 MJ

35 500 MJ ≠ 40 000 MJ

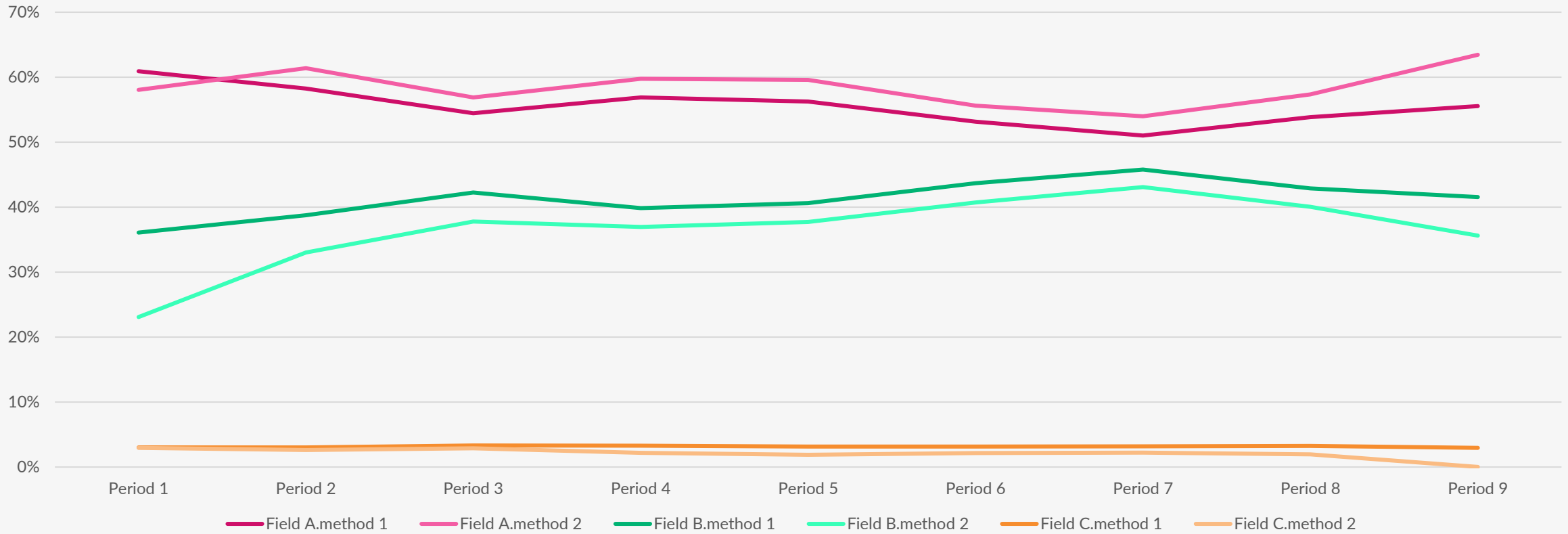
Image source: Wikipedia



Electrical power allocation

Detailed vs. simplified calculations

Electrical power share

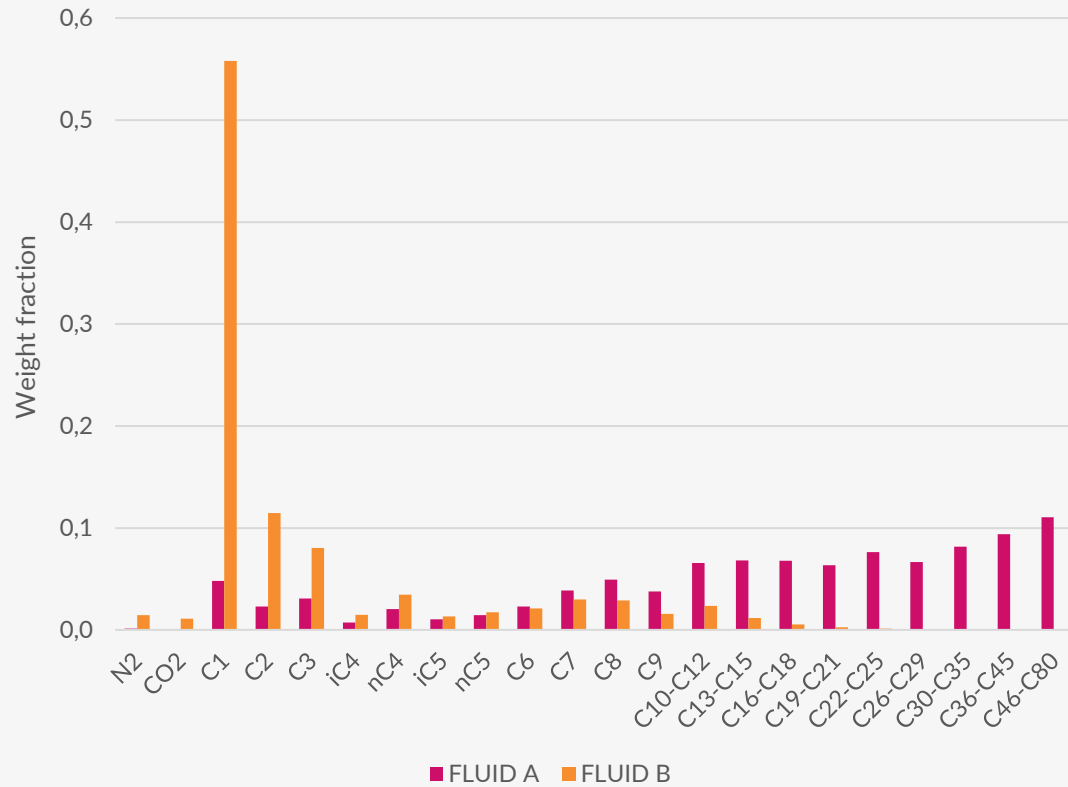




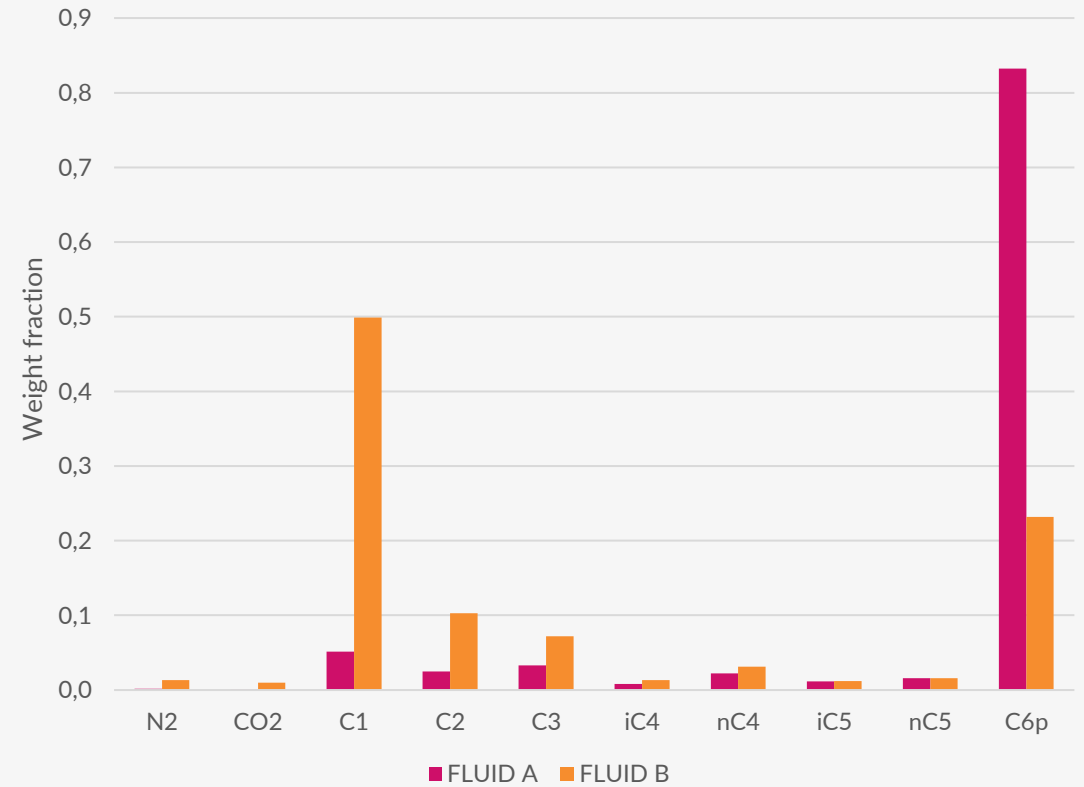
Component Oil Recovery Factor simulation

Ref. [Folgerø, K., et al. \(2021, Oct 25-29\) Influence of fluid compositions and process parameters. NSFMW 2021: Tønsberg, Norway.](#)

Composition



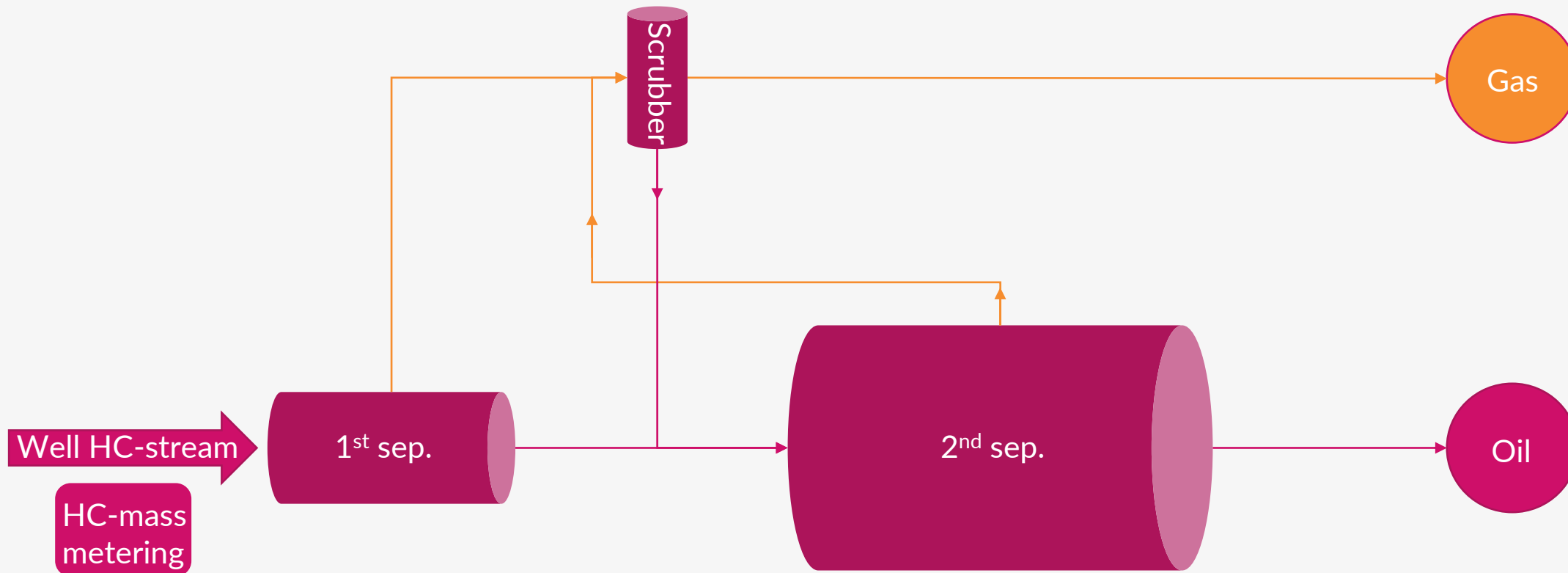
Composition





Component Oil Recovery Factor simulation

Process



CORF vs. component lumping to C6p

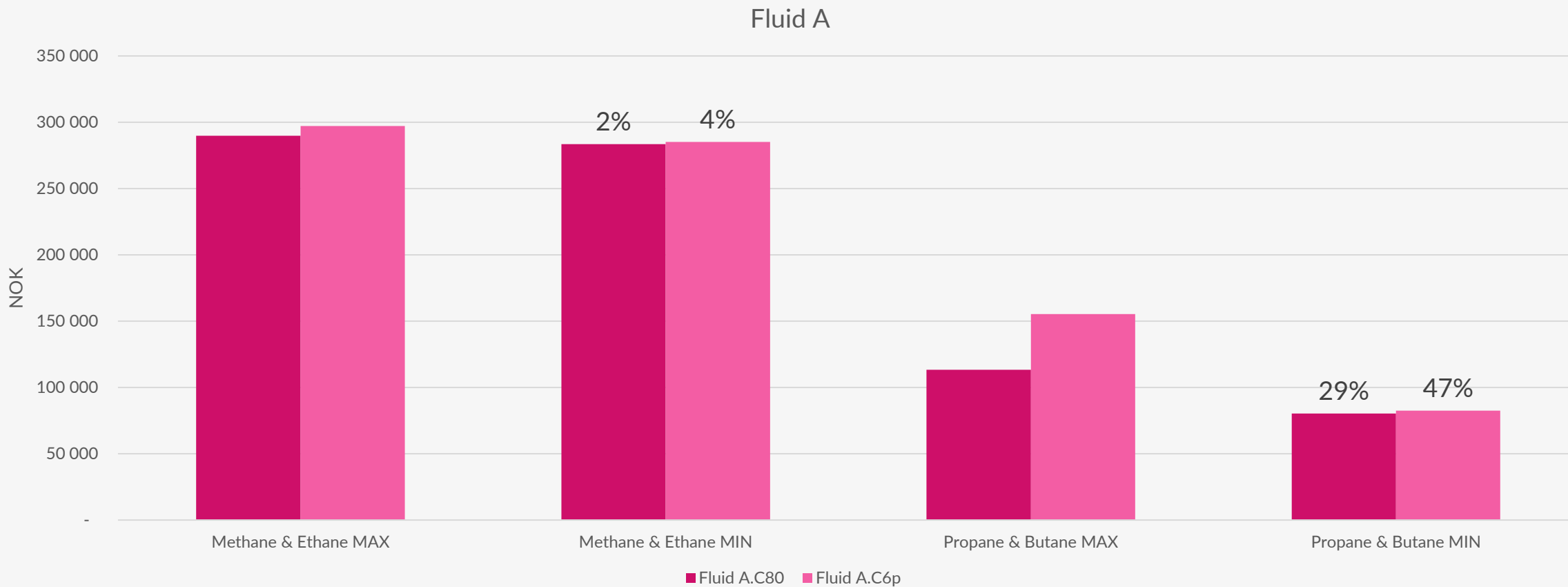
Observations

- Both fluids:
 - Temperature-dependant
- Fluid A (oil-dominant):
 - Most sensitive to 1st separator temperature for both C80 and C6p, slightly amplified dependency with C6p
 - Iso-butane becomes minorly dependant on 2nd sep. pressure
 - Increase in sensitivity to 1st separator temperature
 - Pentane: twofold
- Fluid B (gas-dominant):
 - Most sensitive to 2nd separator temperature for C80
 - Most sensitive to 1st separator temperature for C6p
 - Increase in sensitivity to 1st separator temperature
 - Butane: fourfold
 - Pentane: fivefold



Daily gas values due to CORF

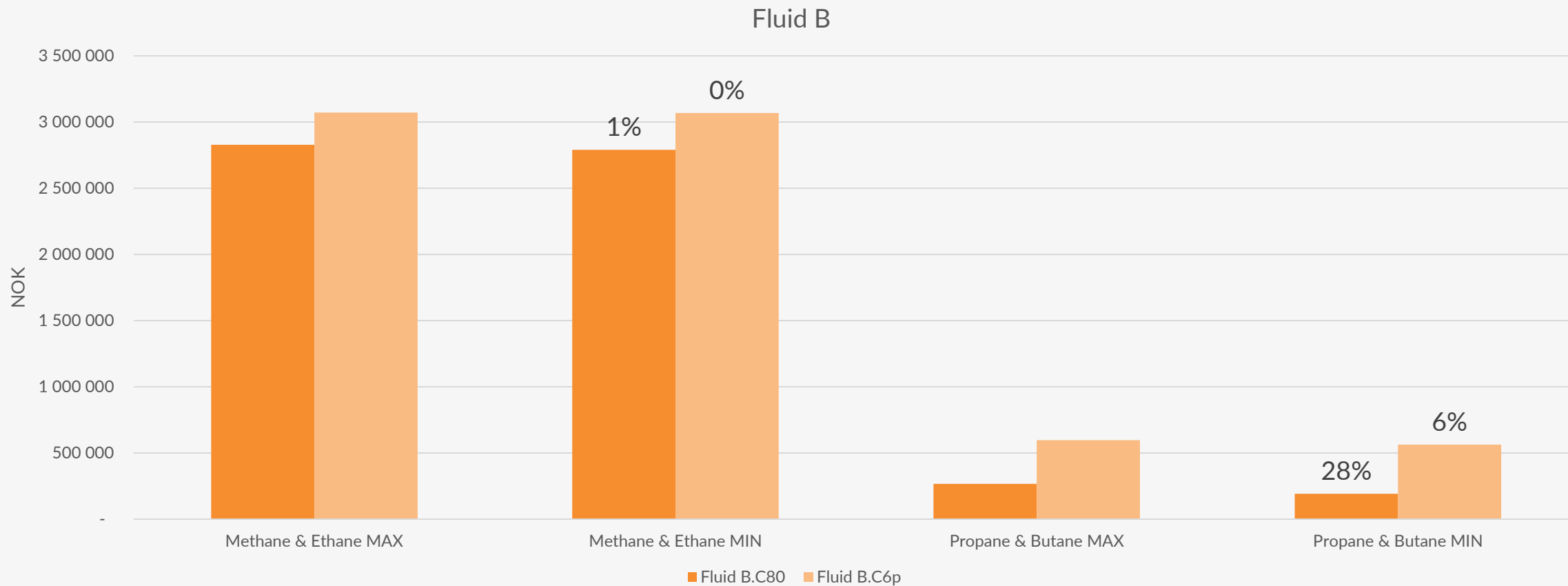
Fluid A (oil-dominant)





Daily gas values due to CORF

Fluid B (gas-dominant)



Conclusions and last thoughts

- Nomenclature and precise formulation in commercial agreements is key
 - allocation procedure, deferral, tariff, OPEX, ...
- CORF: proper input and QC of simulation results extremely important
 - Be aware of differences in gas- and oil-dominant streams dependencies to process conditions when considering allocation systems based on simulations
- Allocation professionals: the devil is not in all of the details, so think cost/benefit!
- Commercial professionals: involve allocation experts to solve that Rubik's cube as early as possible!



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